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(54) **New extractive process for the recovery of naturally occurring macrolides.**

(57) This invention concerns a process for separating a macrolide from acidic, basic and non-polar neutral impurities present in a macrolide containing solution which comprises one or more of the following processes in any order :

a. a solution of said macrolide in a water-immiscible solvent is extracted with aqueous base to substantially remove all acidic impurities ;

b. a solution of said macrolide in a water-immiscible solvent is extracted with aqueous acid to substantially remove all basic impurities ;

c. a solution of said macrolide is subjected to one or more of the following in order to remove non-polar neutral impurities :

(i) extraction with a non-aromatic hydrocarbon solvent in which the macrolide is insoluble,

(ii) treatment with a sufficient quantity of a miscible macrolide non-solvent to cause the macrolide to become insoluble in the resulting solvent mixture and thus separate from the solution whereby the macrolide can be separated from the solvent mixture,

(iii) triturate with a macrolide crystallizing solvent.

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This invention relates to an extractive process for the recovery of naturally occurring macrolides more particularly to a process for separating a naturally occurring neutral macrolide, especially a tricyclic macrolide such as rapamycin, 32-desmethyrapamycin, 15-deoxorapamycin, or FK-506, from other naturally occurring components that are obtained by fermentation processes. More specifically, this invention relates to a process for recovering the tricyclic macrolide rapamycin from fermentation broth extract concentrate and from mother liquor concentrate.

The tricyclic macrolides exemplified by rapamycin and FK-506 have immunosuppressant activity as well as antibiotic and other pharmacological activities and are useful in treating graft and transplant rejections, diseases of inflammation, and autoimmune diseases such as lupus, rheumatoid arthritis, diabetes mellitus and multiple sclerosis.

The tricyclic macrolides rapamycin, 32-desmethyrapamycin, 15-deoxorapamycin and FK-506 are produced by fermentation of various strains of *Streptomyces* under the proper conditions and are neutral as there is no basic amino group, phenolic or carboxylic acid groups present. Rapamycin is produced by culturing *S. hygroscopicus* NRRL 5491 in an aqueous medium. Mycelia containing the tricyclic macrolide are recovered from the growth medium and extracted with an organic solvent such as methanol to obtain a mixture comprised of the desired tricyclic macrolide, related compounds, acidic compounds such as fatty acids, basic compounds such as alkaloids and peptides, and neutral lipophilic compounds such as fats. Typically, the fermentation broth extract is concentrated to facilitate transportation and/or storage until the macrolide can be isolated. Isolation and purification of the tricyclic macrolides from the fermentation broth extract has been, prior to this invention, a laborious expensive process employing various chemical and chromatographic techniques to obtain purified material. [U.S. 5,091,389; U.S. 3,993,749; WO 93/11130; Sehgal, J. of Antibiotics 28(10)727(1975)]. The fermentation broth extract concentrate for rapamycin contains only 5 to 15% rapamycin and up to about 50% acidic components, for example, and rapamycin must be separated from the other components. Typically, processes for recovery of the tricyclic macrolides from fermentation broth extracts involves adsorption on and desorption from activated carbon, selective solubility procedures, and one or more time consuming and expensive chromatographic procedures using column chromatography and/or high pressure liquid chromatography. Heretofore, acidic or basic conditions have been avoided as tricyclic macrolides such as rapamycin are considered to be unstable under acidic or basic conditions. Rapamycin in water-miscible solution, i.e., in methanol or tetrahydrofuran, undergoes degradation by inorganic bases such as aqueous sodium hydroxide, organic bases such as 4-dimethylaminopyridine (DMAP) or 1,8-diazobicyclo[5.4.0]undec-7-ene (DBU) or aqueous mineral acids such as hydrochloric acid and Lewis acids such as zinc chloride [Steffan *et al.*, Tetrahedron Letters (in press), D. Yohanes and S. J. Danishefsky, Tetrahedron Letters 33(49), 7469-7472 (1992); Luengo *et al.*, Tetrahedron Letters 34(6), 991-994 (1993) and D. Yohannes *et al.*, Tetrahedron Letters 34(13), 2075-2078 (1993)].

This invention provides a relatively fast and efficient process for recovery of a macrolide, especially a tricyclic macrolide, from a solution containing impurities and more specifically rapamycin, from fermentation broth extract concentrates and mother liquors or concentrates thereof obtained from recrystallization solvents, triturations and product washings and avoids the time consuming and expensive chromatographic separations exemplified in U.S. 5,091,389; U.S. 3,993,749; WO 93/11130; and Sehgal, J. of Antibiotics 28(10)727(1975).

Accordingly this invention provides a process for separating a macrolide from acidic, basic and non-polar neutral impurities present in a macrolide containing solution which comprises one or more of the following processes in any order:

- a. a solution of said macrolide in a water-immiscible solvent is extracted with aqueous base to substantially remove all acidic impurities;
- b. a solution of said macrolide in a water-immiscible solvent is extracted with aqueous acid to substantially remove all basic impurities;
- c. a solution of said macrolide is subjected to one or more of the following in order to remove non-polar neutral impurities:
 - (i) extraction with a non-aromatic hydrocarbon solvent in which the macrolide is insoluble,
 - (ii) treatment with a sufficient quantity of a miscible macrolide non-solvent to cause the macrolide to become insoluble in the resulting solvent mixture and thus separate from the solution whereby the macrolide can be separated from the solvent mixture,
 - (iii) trituration with a macrolide crystallizing solvent.

In one aspect the process comprises separation of the acidic and/or basic components from the neutral components by dissolving the macrolide-containing concentrate in a suitable water-immiscible solvent and extracting the acidic and/or basic components into aqueous base or acid respectively, and employing selective solubility or extraction techniques to separate the neutral non-polar tricyclic macrolide from the non-polar neutral materials present in the concentrate. While the process described herein is particularly suited to concentrates of fermentation broth extracts or mother liquors, the whole extract solution or mother liquor solutions

can be used in the process of this invention provided the solvent or solvent mixture used for the fermentation broth extraction or recrystallization, trituration or washings is amenable to the process and the volume of the solvent is not cumbersome. Solvent volume may be reduced by partial concentration. Any of the solutions to which the process of this invention may be applied may be referred to as a macrolide containing solution or concentrate.

The product obtained by said process can be purified to acceptable purity by standard procedures known to those skilled in the art.

As used herein, a non-polar solvent is a non-aromatic hydrocarbon solvent such as cyclohexane, cyclohexene, hexane, heptane, pentane and the like. Solvents which are immiscible with the non-aromatic hydrocarbon solvent include but are not limited to acetonitrile and dimethylformamide. The term extraction refers to the procedure of thoroughly mixing one solution with another immiscible solution, allowing the immiscible solutions to separate one from the other and physically removing one layer or phase from the other, and repeating if required. The term wash when referring to a solution refers to the extraction procedure and when referring to a solid, means to rinse the solid with a solvent in which the solid is substantially insoluble. The term mother liquor refers to the organic solvent solutions obtained from crystallization filtrates, washings and back extractions of aqueous extracts and washings and triturations of collected solids. A macrolide solvent is a solvent or solvent mixture which will dissolve the macrolide and accompanying impurities such as the acidic or basic components. A macrolide non-solvent is a solvent or solvent mixture in which the macrolide is substantially insoluble but one in which neutral components such as fats are soluble. A macrolide crystallizing solvent is a solvent or solvent mixture from which the macrolide can be recrystallized or crystallized from an amorphous state upon trituration. Where the process requires the concentration of a solution, it is preferred that the solvent or solvent mixture have sufficient volatility so as to distill off under non-degrading conditions of temperature and pressure.

This invention also provides a process wherein the non-polar neutral components of the macrolide-containing fermentation broth extract concentrate or mother liquor concentrate are removed by extraction of a solution of said concentrate in a first solvent (e.g. acetonitrile, DMF) with a second non-aromatic hydrocarbon solvent immiscible with the first solvent and in which the macrolide is insoluble (e.g. cyclohexane, cyclohexene, hexane, heptane or pentane).

Also provided is a process wherein the water-immiscible solution containing the macrolide after extraction of acid and/or basic components is either

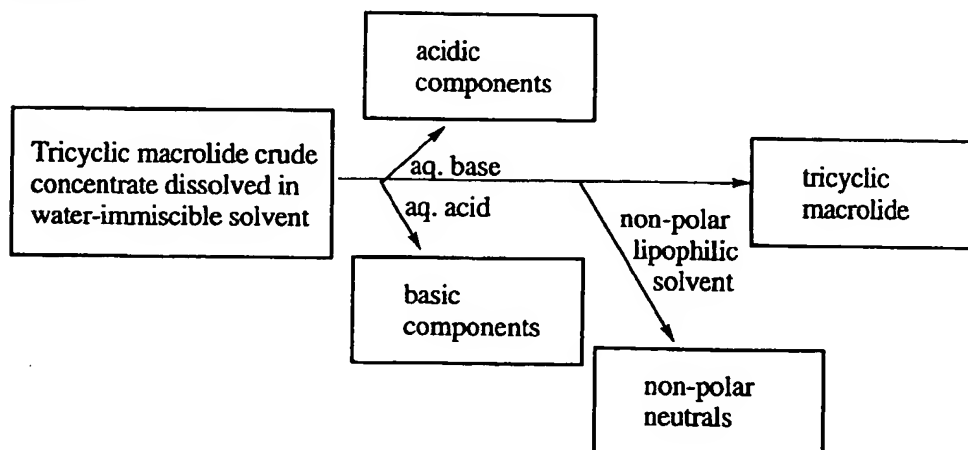
(i) treated with a sufficient quantity of a miscible macrolide non-solvent to cause the macrolide to become insoluble in the resulting solvent mixture and thus separate from the solution whereby the macrolide can be separated from the solvent mixture or

(ii) concentrated and the residue crystallized by admixture with a crystallizing solvent or solvent mixture.

The water-immiscible solution containing the macrolide after extraction of acid and/or base components may also be concentrated and the residue dissolved in a first solvent and extracted with a second non-aromatic hydrocarbon solvent immiscible with the first solvent and in which the macrolide is insoluble to remove the neutral non-polar impurities.

A preferred process of this invention is outlined in the Scheme 1 below:

Scheme 1.



According to the process, the concentrate containing the macrolide, whether from fermentation broth extract concentrate or concentrates from recrystallization and/or wash solvents, is dissolved in a water-immiscible solvent or solvent mixture selected for ability to dissolve the concentrate and ease of removal, including but not limited to dichloromethane, t-butyl methyl ether, ethyl acetate, toluene, 1-butanol, an ethyl acetate/toluene mixture, a heptane/ethyl acetate mixture, or a hexane/methylene chloride mixture. Aqueous solutions of base, including sodium hydroxide, sodium bicarbonate, sodium carbonate, ammonium hydroxide and the like, preferably sodium hydroxide, in concentrations ranging from 0.1 to 5N, preferably from about 0.1 to 1.0N, most preferably 0.1 to 0.5N, are useful for extracting the acidic components. Organic bases such as triethylamine are not as effective as the stronger aqueous inorganic bases in removing the acidic components. Aqueous solutions of mineral acid, including hydrochloric acid, monopotassium phosphate, monosodium sulfate and the like, preferably hydrochloric acid, in concentrations of from 0.1 to 5N, are useful for extracting the basic components. Organic acids, such as trifluoroacetic acid are not as effective as the mineral acids in removing the basic components. Extractions of acidic and/or basic components from the solution containing the macrolide are conveniently carried out between -5°C and 45°C, preferably -5°C and 30°C, most preferably in the range of -5 to 10°C. To avoid possible degradation of the macrolide by the acid or base, the extraction process should be completed without delay. Depending on the amounts of acidic and/or basic components present, extraction of both acids and bases may not be necessary and extraction of the acidic components alone or basic components alone may be sufficient in removal of enough impurity from the macrolide containing solution to permit isolation of the tricyclic macrolide.

It is advantageous to remove the acidic (or basic) components from the solution of macrolide-containing concentrate in one time-saving extraction step. The amount of aqueous base (or acid) needed so that excess base (or acid) is available in the extraction process can be determined by extracting an aliquot taken from the solution of the macrolide containing concentrate with aqueous base (or acid) and determining the volume of aqueous base (or acid) required to give an extract of the aliquot having a pH such that a stoichiometric excess of base (or acid) is available. The excess of acid or base is determined by using a pH meter or other means of determining pH. The volume of aqueous base (or acid) needed to extract the solution from which the aliquot was taken is then proportional to the ratio of the volumes of neutral macrolide containing solution to be extracted and the aliquot taken therefrom. Thus extraction of acidic (or basic) components can be done in one operation rather than performing multiple extractions with less than sufficient amounts of aqueous base (or acid). Obviously where both acidic and basic components are to be removed from the solution of the macrolide containing concentrate, separate extractions with aqueous base and aqueous acid respectively will have to be performed. With solutions of rapamycin containing concentrate, for instance, one extraction with aqueous sodium hydroxide solution sufficient to have a final pH of 12 is sufficient to remove substantially all of the acidic components.

The macrolide recovered from solution using the above processes can be purified to the degree of purity desired by conventional purification techniques known to those skilled in the art. The filtrates and washings may be reworked to recover additional macrolide if desired.

After performing the extraction procedures to remove the acidic and/or basic components from the water-immiscible solvent solution containing the macrolide, the macrolide may be separated from the non-polar neutral components by one of the following methods:

(1) A macrolide non-solvent (or solvent mixture), miscible with said macrolide containing water-immiscible solvent solution from which the acidic and/or basic components were extracted, is added to the macrolide containing solution in sufficient quantity so as to render the macrolide and perhaps macrolide-related products insoluble in the resulting solution and form a separate phase, either an oil or a solid, which may then be separated by ordinary separation techniques known to those skilled in the art.

(2) The water-immiscible solvent solution containing the neutral macrolide from which the acidic and/or polar components were extracted is concentrated and the residual material containing the macrolide is dissolved in a macrolide dissolving solvent such as acetonitrile or dimethylformamide and extracted with a non-aromatic hydrocarbon solvent such as cyclohexane, hexane, heptane or cyclohexene. The macrolide-dissolving solvent layer is separated and concentrated. The residue containing the macrolide is then triturated with a crystallizing solvent to obtain the macrolide if said macrolide is a solid or purified by techniques known to those skilled in the art such as chromatography if the macrolide is an oil. Alternatively, the macrolide-dissolving solvent, after extraction with the non-aromatic hydrocarbon solvent may be treated with a miscible non-macrolide dissolving solvent as in procedure (1) above.

(3) The macrolide containing water-immiscible solvent solution from which the acidic and/or basic components were extracted is concentrated and the residual material is triturated with macrolide crystallizing solvent such as diethyl ether, diisopropyl ether or t-butyl methyl ether.

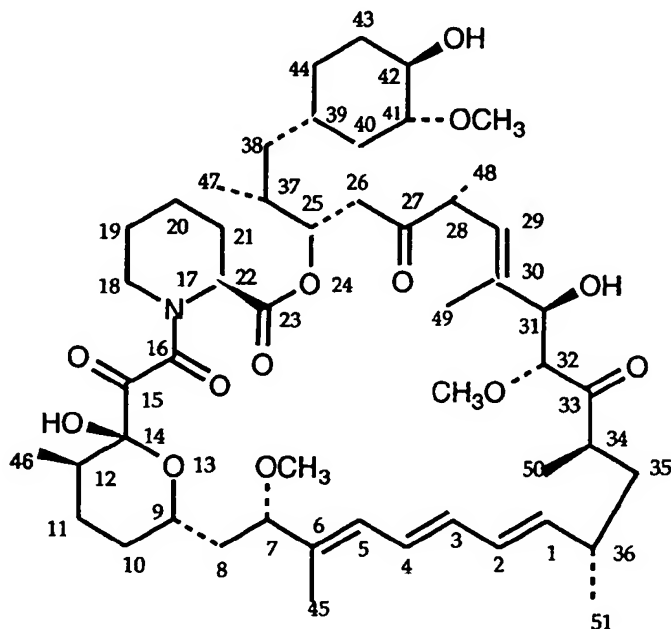
Alternatively, the macrolide containing concentrate can be extracted first according to one of methods (1)

to (3) above to remove non-polar components and then the residue containing the macrolide dissolved in a water-immiscible solvent if not already in such a solvent and extracted with aqueous base and/or acid to remove the acidic and/or basic components.

The above process takes advantage of the unexpected finding that macrolides such as the tricyclic macrolide rapamycin do not decompose when subjected to aqueous acid or base extraction procedures under proper temperature conditions from water-immiscible solvent solutions of macrolide containing concentrates. It was previously thought that degradation would occur, based on the observed degradation of rapamycin that results from acid or base exposure in solution.

This extraction process greatly shortens the time necessary to recover macrolides from said concentrates and avoids the time-consuming and expensive chromatographic processes.

The tricyclic macrolide rapamycin is a crystalline solid soluble in methanol, acetone, dimethylformamide, slightly soluble in diethyl ether and is sparingly soluble in hexane or petroleum ether and is insoluble in water. Rapamycin has the structure shown below. The atom numbering system is that used by Chemical Abstracts.



The structures of 32-desmethylrapamycin and 15-deoxorapamycin can easily be discerned from the above structure of rapamycin. The structure of the neutral tricyclic macrolide FK-506 is shown below.

Example 4

A solution of concentrated fermentation broth extract (100.0 g, 11.8% rapamycin content) taken up in ethyl acetate (400 mL) was washed with one 200 mL portion and two 100 mL portions of 0.5 N NaOH solution at 0-5°C and then washed with two 200 mL portions of 0.5 N hydrochloric acid solution at 0-5°C and finally washed with water until the wash was neutral. The aqueous washings were back extracted with ethyl acetate (100 mL) and the ethyl acetate solutions combined. The ethyl acetate solution was concentrated and the residue (43.2 g) triturated with diisopropyl ether (45 mL). The crystalline solid was collected, washed with diisopropyl ether and dried to yield 9.5 g of rapamycin (85.3% purity, 68.7% yield). The diisopropyl ether filtrates were concentrated to give an oil (31.6 g) with a 6.6% rapamycin content.

Example 5

A solution of concentrated fermentation broth extract (25.2 g, 10.4% rapamycin content) taken up in a mixture of toluene (120 mL) and ethyl acetate (25 mL) was washed sequentially with three 50 mL portions of 0.5 N NaOH solution at 0-5°C, twice with two 50 mL portions of 0.5 N hydrochloric acid at 0-5°C, and then with water until the wash was neutral. The toluene/ethyl acetate solution (128 mL) was divided into two equal portions for further treatment by the following methods:

Method A. The toluene/ethyl acetate solution (64 mL) was concentrated and the residue (5.7 g) triturated with diethyl ether (11 mL). The crystalline solid was collected, washed with additional diethyl ether, and dried to give 0.84 g of rapamycin (92.7% purity, 64.1% yield). Concentration of the diethyl ether filtrates gave 4.3 g of an oil having a 6.8% rapamycin content.

Method B. The toluene/ethyl acetate solution (64 mL) was concentrated and the residue (9.0 g) was dissolved in acetonitrile (50 mL). The acetonitrile solution was washed with two 25 mL portions of cyclohexane. The acetonitrile solution was then concentrated and the residue (4.3 g) triturated with diethyl ether (11 mL). The crystalline solid was collected, washed with diethyl ether, and dried to yield 0.81 g of rapamycin (94.6% purity, 61.8% yield). Concentrations of the diethyl ether filtrates gave 3.0 g of an oil having a 5.9% rapamycin content.

Example 6

Mother liquor concentrate (996.0 g, 21.6% rapamycin content) was triturated with t-butyl methyl ether (4000 mL). The crystalline solids were collected, washed with t-butyl methyl ether (500 mL), and dried to yield 36.2 g of rapamycin (95.1% purity, 13.8% yield). The filtrates were washed with one 2000 mL portion and two 1000 mL portions of 0.5 N sodium hydroxide solution at 0-5°C. The combined base extract was washed once with t-butyl methyl ether (500 mL). The t-butyl methyl ether filtrate and extract were combined and washed with water until the wash was neutral. The water extracts were combined and extracted with t-butyl methyl ether (500 mL). The t-butyl methyl ether solutions were combined, concentrated, and the residue (377.1 g) triturated with diisopropyl ether (350 mL). The crystalline solids were collected, washed with diisopropyl ether, and dried to give 126.7 g of rapamycin (82.4% purity, 58.9% yield). Thus the total recovery of rapamycin from the mother liquor concentrate was 162.9 g (72.7%). Concentration of the diisopropyl ether filtrates gave 157.9 g of oil having a 20.9% rapamycin content.

Example 7

A solution of mother liquor concentrate (562.1 g, 21.6% rapamycin content) taken up in dichloromethane (2000 mL) was washed with three 500 mL portions of 0.5 N sodium hydroxide solution at 0-5°C and the combined aqueous basic extracts were extracted with one 200 mL portion of dichloromethane. The organic solutions were combined and washed with two 500 mL portions of 0.5 N hydrochloric acid solution at 0-5°C. The combined aqueous acid extracts were extracted with one 200 mL portion of dichloromethane. The combined organic extracts were washed with water until the wash water was neutral. The organic solution was concentrated and the residue (255.0 g) was triturated with diisopropyl ether (250 mL). The crystalline solids were collected, washed with diisopropyl ether and dried to give 108.6 g of rapamycin (86.6% purity, 77.4% recovery). Concentration of the diisopropyl ether filtrates gave 100.2 g of oil having a 23.1% rapamycin content.

Example 8

Aqueous 0.5 N sodium hydroxide (400 mL) at 0-5°C was added to a vigorously stirred chilled (0-5°C) sol-

ution of concentrated fermentation broth extract (198.5 g, 8.3% rapamycin content) taken up in 800 mL of t-butyl methyl ether at such a rate so that the temperature could be maintained at 0-5°C. After vigorous stirring for 5 minutes, the lower aqueous basic layer was removed and stored at 0-5°C. The organic layer was re-extracted with two 200 mL portions of 0.5 N sodium hydroxide solution at 0-5°C. The aqueous basic extracts were combined and re-extracted with t-butyl methyl ether (200 mL). The t-butyl methyl ether solutions were combined and washed with water until the wash was neutral (pH=7). The aqueous washes were combined and extracted with t-butyl methyl ether (100 mL). The t-butyl methyl ether solutions were combined, washed with saturated aqueous sodium chloride solution, and concentrated under vacuum at 40°C. The residue was triturated with diisopropyl ether (85 mL) at 20-25°C for a minimum of one hour and the mixture cooled to 0-5°C overnight. The crystalline solid was collected using a sintered glass Buchner funnel and washed with a 4:1 mixture of diisopropyl ether - t-butyl methyl ether at 20-25°C (5 x 20 mL or until filtrate was colorless). The crystalline solid is dried to constant weight to yield 12.0 g of rapamycin (91.2% purity, 66.4% recovery). Concentration of the t-butyl methyl ether filtrates and washing gave 63.9 g of a gum having a 3.63% rapamycin content.

Example 9

Mother liquor concentrate (200 g, 25% rapamycin content) was dissolved with stirring in t-butyl methyl ether (800 mL) at room temperature. The stirred solution was cooled to 0-5°C and extracted without delay with 270 mL of 0.65 N sodium hydroxide solution, pre-cooled to 0-5°C, while maintaining the temperature of the mixture at 0-5°C. (The amount of aqueous sodium hydroxide necessary to have a final pH of 12 in the extract was determined on an aliquot of the concentrated mother liquor.)

The aqueous base layer was stored at 0-5°C while the organic layer was washed with 5% sodium chloride solution while maintaining the mixture at 0-5°C. The aqueous basic extract was back extracted with t-butyl methyl ether (100 mL). The organic layers were combined and washed with three 200 mL portions of 5% sodium chloride solution (pH of final wash solution was 7.4). The organic solution was concentrated under reduced pressure (60-130 mmHg) at a temperature of 25-40°C. Cyclohexene (80 mL) was added slowly over 30 minutes to the residue with stirring at room temperature and stirred until crystallization was complete (3 hours). The mixture was stirred at room temperature for one hour more and the mixture chilled to 0-5°C and stirred overnight. The off-white crystalline solid was then collected on a fritted glass Buchner funnel. The solid was washed five times with 40 mL portions of a 2:3 mixture of t-butyl methyl ether and cyclohexene. The solid was dried to constant weight in a vacuum oven at 35-40°C to obtain 22.7 g of rapamycin (90.6% pure, 41.4% recovery). Concentration of the filtrates and washings (t-butyl methyl ether and cyclohexene) gave 60.1 g of an oil having a 37.5% rapamycin content.

Claims

1. A process for separating a macrolide from acidic, basic and non-polar neutral impurities present in a macrolide containing solution which comprises one or more of the following processes in any order:
 - a. a solution of said macrolide in a water-immiscible solvent is extracted with aqueous base to substantially remove all acidic impurities;
 - b. a solution of said macrolide in a water-immiscible solvent is extracted with aqueous acid to substantially remove all basic impurities;
 - c. a solution of said macrolide is subjected to one or more of the following in order to remove non-polar neutral impurities:
 - (i) extraction with a non-aromatic hydrocarbon solvent in which the macrolide is insoluble,
 - (ii) treatment with a sufficient quantity of a miscible macrolide non-solvent to cause the macrolide to become insoluble in the resulting solvent mixture and thus separate from the solution whereby the macrolide can be separated from the solvent mixture,
 - (iii) triturate with a macrolide crystallizing solvent.
2. A process according to Claim 1 in which in step (c) the solution of said macrolide is a solution in a water immiscible solvent.
3. A process according to Claim 1 or Claim 2 in which the extraction of acidic and/or basic impurities is carried out at a temperature from about -5°C to about 45°C.

4. A process according to Claim 1 or Claim 2 in which the extraction of acidic and/or basic impurities is carried out at a temperature from about -5°C to about 10°C.
5. A process according to any one of Claims 1 to 4 wherein the macrolide containing solution is a macrolide-containing fermentation broth extract concentrate or a mother liquor concentrate.
6. A process according to Claim 5 wherein the non-polar neutral components of the macrolide-containing fermentation broth extract concentrate or mother liquor concentrate are removed by extraction of a solution of said concentrate in a first solvent with a second non-aromatic hydrocarbon solvent immiscible with the first solvent and in which the macrolide is insoluble.
7. A process according to Claim 5 wherein the water-immiscible solution containing the macrolide after extraction of acid and/or basic components is treated with a sufficient quantity of a miscible macrolide non-solvent to cause the macrolide to become insoluble in the resulting solvent mixture and thus separate from the solution whereby the macrolide can be separated from the solvent mixture.
8. A process according to any one of Claims 1 to 5 wherein the water-immiscible solution containing the macrolide after extraction of acidic and/or basic components is concentrated and the residue crystallized by admixture with a crystallizing solvent or solvent mixture.
9. A process according to any one of Claims 1 to 5 wherein the water-immiscible solution containing the macrolide after extraction of acid and/or base components is concentrated and the residue is dissolved in a first solvent and extracted with a second non-aromatic hydrocarbon solvent immiscible with the first solvent and in which the macrolide is insoluble to remove the neutral non-polar impurities.
10. A process according to Claim 5 wherein the fermentation broth extract concentrate or mother liquor concentrate is first dissolved in a first solvent and extracted with a second non-aromatic hydrocarbon solvent immiscible with said first solvent, to remove the non-polar neutral impurities, the solution in the first solvent is then concentrated and the residue dissolved in a water immiscible solvent and extracted with aqueous base and/or acid to remove acidic and/or basic impurities.
11. A process according to claim any one of Claims 1 to 10 wherein the non-aromatic hydrocarbon solvent is cyclohexane, cyclohexene, hexane, heptane or pentane or a mixture thereof.
12. A process according to claim any one of Claims 1 to 11 in which the water-immiscible solvent is dichloromethane, t-butyl methyl ether, ethyl acetate, toluene, 1-butanol, an ethyl acetate/toluene mixture, a heptane/ethyl acetate mixture, or a hexane/methylene chloride mixture.
13. A process according to claim any one of Claims 1 to 12 in which the aqueous base is sodium hydroxide, sodium bicarbonate, sodium carbonate or ammonium hydroxide.
14. A process according to claim any one of Claims 1 to 13 in which the aqueous acid is hydrochloric acid, monopotassium phosphate or monosodium sulfate.
15. A process according to any one of Claims 1 to 14 wherein the macrolide is a tricyclic macrolide.
16. A process according to Claim 15 wherein the tricyclic macrolide is rapamycin or a naturally occurring homolog or analog thereof or FK-506 or a naturally occurring homolog or analog thereof.
17. A process according to Claim 15 wherein the tricyclic macrolide is rapamycin, 32-desmethyrapamycin or 15-deoxorapamycin.



European Patent
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EUROPEAN SEARCH REPORT

Application Number
EP 94 30 8107

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. CL.6)
D,A	US-A-3 993 749 (SURENDRA N. SEHGAL ET AL) *Column 3*	1	C07D498/18 C12P17/18
D,A	EP-A-0 510 903 (MERCK & CO. INC.) *Page 7: example 2* & US-A-5 091 389 (ONDEYKA JOHN ET AL)	1	
D,A	WO-A-93 11130 (SMITH-KLINE BEECHAM PLC) *Page 19*	1	
			TECHNICAL FIELDS SEARCHED (Int. CL.6)
			C07D C12P
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 1 February 1995	Examiner Luyten, H
CATEGORY OF CITED DOCUMENTS		T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons A : technological background O : non-written disclosure P : intermediate document & : member of the same patent family, corresponding document	
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